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Description

The present invention relates to a catalyst and process for producing phthalic anhydride by vapor phase catalytic oxidation of o-xylene and/or naphthalene with molecular oxygen or gas containing molecular oxygen.

In recent years, when phthalic anhydride is so produced, an increase in yield is attempted, after obtaining a crude product at first, by treating it with heat and subjecting it to distillation. Since this process is simple and facile to perform, it can be expected that a cheap product of high quality is produced on a large scale.

Furthermore, as a means to elevate the yield, there is stabilized production resulting from maintaining reaction conditions and catalytic activity. An example of this process is an oxidation reaction carried out under high load reaction conditions such as high concentration of starting material gas. However, production of phthalic anhydride from o-xylene or naphthalene is accompanied by violent heat generation and, under high concentration conditions, temperature rise at a hot spot is extreme, so that excessive oxidation occurs, the yield of phthalic anhydride is lowered, and deterioration of the catalyst is extremely accelerated. Catalysts capable of withstanding such high load reaction conditions have been already proposed, for example, in U.S.P. 4,356,112.

A widely known catalyst of this kind is a catalyst for producing phthalic anhydride, having supported on an inactive carrier a catalytic active substance containing vanadium oxide and titanium oxide as main components. Catalysts of the type are disclosed, for example, in G.B. 1,203,321, U.S.P. 4,046,780, Japanese Examined Patent Publication of showa 49-41036, U.S.P. 3,843,552, U.S.P. 3,909,457, and Japanese Unexamined Patent Publication of showa 57-105241. These catalysts have their respective features and some of them have been proved useful by being applied industrially.

There is, however, ample room for improvement of catalyst performance; an increase in yield of only 1 % is notable in its economic effect considering the scale of production.

EP-A-0003158 discloses a catalyst for oxidation of hydrocarbons which contains Ti and V oxides and Sb_2O_5 .

The present invention provides a catalyst further improved in catalyst performance compared with hitherto-known conventional catalysts for producing phthalic anhydride. The catalyst makes it possible to produce phthalic anhydride with high selectivity even under high load and high temperature conditions, is durable, and can produce phthalic anhydride under stable conditions for a long period.

The present inventors have found by extensive research that improvement is attained, especially under a high temperature condition, by using a five-valent antimony compound such as represented by Sb_2O_5 as a starting material, instead of a conventional trivalent antimony compound such as represented by Sb_2O_3 , in introducing antimony into a vanadium-titanium-based catalyst as an ingredient of the catalytic active composition.

The five-valent antimony compound such as represented by Sb_2O_5 can be used as starting material to introduce antimony even in a vanadium-titanium-based catalyst in to which silver has been already added.

The first invention provides a catalyst for producing phthalic anhydride by vapor phase catalytic oxidation of o-xylene and/or naphthalene with molecular oxygen or gas containing molecular oxygen, having supported on a heat-resistant inorganic carrier a catalytic active substance;

which comprises (A) 1 to 20 parts by weight of vanadium oxide as V_2O_5 , and 99 to 80 parts by weight of anatase type titanium dioxide with specific surface area of 10 to 60 m^2/g as TiO_2 ; and (B), per 100 parts by total weight of (A), 0.01 to 1 part by weight of niobium as Nb_2O_5 , 0.05 to 2 parts by weight of at least one element selected from potassium, cesium, rubidium and thallium as oxide, 0.2 to 1.2 parts by weight of phosphorus as P_2O_5 , 0.55 to 5.5 parts by weight of antimony as Sb_2O_5 ; and wherein a five-valent antimony compound is used as an antimony source in production of the catalytic active substance.

Hereinafter, this obtained catalyst is referred to as catalyst 1.

The second invention provides a catalyst for producing phthalic anhydride by vapor phase catalytic oxidation of o-xylene and/or naphthalene with molecular oxygen or gas containing molecular oxygen, having supported on a heat resistant inorganic carrier a catalytic active substance;

which comprises (A) 1 to 20 parts by weight of vanadium oxide as V_2O_5 , and 99 to 80 parts by weight of anatase-type titanium dioxide with specific surface area of 10 to 60 m^2/g as TiO_2 ; and (B), per 100 parts by total weight of (A), 0.01 to 1 part by weight of niobium as Nb_2O_5 , 0.05 to 2 parts by weight of at least one element selected from potassium, cesium, rubidium and thallium as oxide, 0.2 to 1.2 parts by weight of phosphorus as P_2O_5 , 0.05 to 2 parts by weight of silver as Ag_2O , 0.55 to 5.5 parts by weight of a five-valent antimony compound as Sb_2O_5 , and wherein a five-valent antimony compound is used as an antimony source in production of the catalytic active substance.

Hereinafter, this obtained catalyst is referred to as catalyst 2.

It is one of the features of the invention that anatase type titanium dioxide with specific surface area of 10 to 60 m²/g, preferably 15 to 40 m²/g, is used as an ingredient of the catalytic active substance. If the specific surface area of the anatase type titanium dioxide is less than 10 m²/g, the activity of the obtained catalyst is low; when it exceeds 60 m²/g, the durability of the catalyst is reduced and the yield rapidly decreases, which is not preferable (the specific surface area is measured by the BET method).

Although there are a so-called solution method and so-called " solidifying method " as methods for producing the anatase type titanium dioxide, the solution method is preferred for use.

According to the solution method, ilmenite (FeOTiO₂) is treated with aqueous sulfuric acid of about 70 to 80 % concentration, hydrolyzed under pressure at about 150 °C, and calcined to obtain anatase type titanium dioxide. The obtained anatase type titanium dioxide is high in mechanical strength in spite of porosity; it possesses such strength as to be regarded as " primary particles " not crushed by mechanical grinding by an ordinary ball mill or the like. Although this anatase type titanium dioxide has a large average particle size of 0.4 to 0.7 μm, it has such a large specific surface area as 10 to 60 m²/g, and it is essentially an assembly of primary particles of small diameter (the average particle size is measured by a transmission electron microscope). Among the particles, the ones having a sphere shape are preferred for practical use.

Furthermore, the solidifying method is somewhat inconvenient in practical use because this method is performed in sulfuric acid of higher concentration compared with the solution method.

Due to an ore used as a starting material, there is a case where iron, zinc, aluminum, manganese, chromium, calcium, lead and so forth mingle in the anatase type titanium dioxide, however, as far as they are 0.5 % by weight or less as oxide against the titanium dioxide, there is no problem on the catalytic performance.

The heat-resistant inorganic carrier used in this invention is required to be stable for a long period of time at a temperature sufficiently higher than the catalyst-calcining temperature as well as at a temperature of the catalyst in producing phthalic anhydride and also, it is required to be unreactive with the catalytic active substance. Preferable examples of heat-resistant inorganic carriers of this kind are silicon carbide (SiC), alumina, zirconium oxide, titanium oxide and the like.

Among these carriers, the silicon carbide carrier is very preferable and, a preferable alumina (Al₂O₃) content in this silicon carbide is 20 % by weight or less and its further preferable content is 5 % by weight or less. A further preferable carrier is a silicon carbide carrier obtained by self-sintering of silicon carbide powder with a purity of 98 % or more. A preferable apparent porosity of the silicon carbide carrier is 10 % or more and a further preferable one is a range of from 15 to 45 %.

The shape of the heat-resistant inorganic carrier is not particularly limited, but a spherical or columnar shapes are easy to handle and such a carrier as having an average diameter of 2 to 15 mm is preferable for use.

A feature of the catalyst relating to this invention is to use a five-valent antimony compound such as represented by Sb₂O₅ as an antimony source, that is one ingredient of the catalytic active substance, and the antimony compound is properly selected from various kinds of five-valent antimony-containing compounds in addition to the Sb₂O₅. An amount for use of the antimony compound is 0.55 to 5.5 parts by weight as Sb₂O₅ per 100 parts by weight of the sum of the two ingredients, that are vanadium oxide and anatase type titanium dioxide: a preferable amount for use is 1.5 to 3.5 parts by weight as Sb₂O₅. If the content of antimony is too much or too small, the object of this invention is not attained.

Preferable five-valent antimony-containing compounds are such as having an average particle size in a range of from 1 to 40 μm and further preferable ones are such as having the size in a range of from 5 to 30 μm. If the average particle size is larger than 40 μm, activity deviation becomes large in converting the five-valent antimony-containing compound into a catalyst with other ingredients. That is due to difficulty in keeping the most suitable temperature at constant. This may arise from uneven distribution of antimony particles in the catalyst-active layer. Also, if the average particle size is smaller than 1 μm, the catalyst activity becomes higher than a case where particles having an average particle size of 1 μm or larger and also, the effect of adding five-valent antimony becomes low. This may be because the reaction activity on the surface of the five-valent antimony-containing compound itself is high. (The average particle size is determined by a transmission electron microscope before preparing the catalyst.)

The vanadium, niobium, potassium, cesium, rubidium, thallium and phosphorus starting materials for preparing the catalyst may be selected from, aside from such oxides as V₂O₅, Nb₂O₅, K₂O, Cs₂O, Rb₂O, Tl₂O and P₂O₅, compounds transformed to such oxides by heating such as ammonium salts, nitrates, sulfates, halides, organic acid salts and hydroxides of the individual elements.

A preferable total amount for use of the potassium, cesium, rubidium and thallium is, per 100 parts by total weight of vanadium oxide and anatase type titanium dioxide, 0.05 to 2 parts by weight as the forementioned respective oxides, and a preferable amounts for use of p and Nb are respectively 0.2 to 1.2 parts by weight as P_2O_5 and 0.01 to 1 part by weight as Nb_2O_5 . If the content is too much or too small, the object of this invention is not attained.

Concerning the catalyst 2 relating to the present invention, silver is one additional ingredient, aside from the catalytic active substances shown in the catalyst 1.

As for the silver ingredient, aside from Ag_2O , a nitrate, halide, an ammonium salt, organic acid salt, a hydroxide, an amine complex, a phosphate, sulfide and the like may be used. Some of them, such as silver halide and silver phosphate, are not transformed into oxide by heating in the production of the catalyst, but all of them may be used in this invention without trouble.

A preferable amount for use of silver is, per 100 parts by total weight of vanadium oxide and anatase type titanium dioxide, 0.05 to 2 parts by weight as Ag_2O . If the content is too much or too small, the object of this invention is not attained.

In a case where silver phosphate is used, because this compound consists of phosphorus and silver and does not contribute as a phosphorus additive, the phosphorus in silver phosphate is not included in the forementioned phosphorus content of 0.2 to 1.2 parts by weight as P_2O_5 .

Although the amount of a catalytic active substance to be supported on the heat-resistant inorganic carrier varies with the carrier size, and a preferable amount is 3 to 20 g per 100 cc of the carrier. The catalytic active substance layer obtained by supporting the catalytic active substance on the carrier has preferably a surface such that the pore volume occupied by pores of 0.15 to 0.45 μm diameter is 50% or more, preferably 75% or more, of the total fine pore volume occupied by pores of 10 μm or less diameter (the pore volume is obtained from a pore-diameter distribution measured by a mercury injection porosimeter). The object of this invention is more effectively attained by arranging a catalytic active substance layer having such surface characteristic as mentioned above.

The method of supporting the catalytic active substance on a heat-resistant inorganic carrier in production of catalysts of this invention is not particularly limited, and various known methods can be used. The most simple method is to put a specific amount of carrier into a rotary drum which can be heated from outside and, while keeping it at a temperature of 200 to 300 °C, to spray a slurry containing the catalytic active substance on the carrier to support the substance.

A practical method of arranging a catalytic active substance layer having such surface characteristics as mentioned above is mentioned. When a slurry is prepared by using anatase type titanium dioxide with a primary particle size of 0.005 to 0.05 μm , the slurry concentration is adjusted at 5 to 25 % by weight, preferably 10 to 20 % by weight; and when using anatase type titanium dioxide with a primary particle size greater than 0.05 μm , the slurry concentration is adjusted at 10 to 40 % by weight, preferably 15 to 25 % by weight; and the slurry obtained is made sufficiently uniform by using an emulsifier, a heat-resistant inorganic carrier is placed into a rotary drum kept at a temperature of 200 to 300 °C, the forementioned slurry is sprayed with rotating the drum so that a catalytic active substance can be supported in a defined content, and then a carrier which has supported the active substance is calcined in passing air at a temperature of 450 to 700 °C, preferably 500 to 600 °C, for about 2 to 10 hours to obtain a catalyst of this invention.

The oxidation reaction of o-xylene and/or naphthalene using a catalyst of this invention can be carried out under usual reaction conditions. For example, a reaction tube of inside diameter 5 to 40 mm, preferably 15 to 27 mm, is filled with the catalyst to a height of 1 to 5 m, preferably 1.5 to 3 m, and maintained at a temperature of 340 to 420 °C preferably 360 to 400 °C, by a heating medium. Into this reaction tube, the o-xylene and/or naphthalene is blown, together with air or gas containing 5 to 21 % by volume of molecular oxygen, at a rate of 5 to 70 g per Nm^3 of air or at a rate of 5 to 110 g per Nm^3 of gas containing molecular oxygen, at a spatial velocity of 1,000 to 6,000 hr^{-1} (STP), preferably 1,000 to 4,000 hr^{-1} (STP).

The third and fourth inventions relate to a process by which the catalysts 1 and 2 are used with great advantage. In the inventions, the catalyst layer in a reaction tube is divided into two or more sections to arrange a plurality of reaction zones, a plural piece of catalysts of controlled activity are charged in the reaction zones so that the catalytic activity is higher from the material gas inlet of the reaction tube toward the outlet. Preferably, the reaction tube is divided into two layers, and the inlet part is filled with a defined catalyst (first stage catalyst) to a layer height of 30 to 70 % of the overall catalyst layer height, while the remaining layer height at the outlet is filled with catalyst (second stage catalyst) of higher activity than the first stage catalyst, and thus the catalysts are provided for the oxidation of o-xylene and/or naphthalene.

An example for preparing catalyst 2 of this invention is explained. Catalysts of the same type but different in activity may be easily prepared by changing the content of, for example, phosphorus. Thus,

using 0.2 to 0.4 parts by weight of phosphorus as oxide in the catalytic active substances per 100 parts by total weight of the vanadium oxide and anatase type titanium dioxide, an above first stage catalyst is prepared, and using 0.4 to 1.2 parts by weight, a second stage catalyst of higher activity is prepared.

The catalyst activity may also be controlled by varying the kind and/or content of at least one element selected from potassium, cesium, rubidium and thallium.

Furthermore, a catalyst-filled layer of controlled activity may be made by a joint use of the catalyst 1 and catalyst 2.

By performing the oxidation reaction under such conditions as mentioned above, heat accumulation in the hot spot in the catalyst layer is suppressed and, as a result, catalyst deterioration due to thermal load is reduced, so that long-term stable operation is possible industrially. Excessive oxidation reaction at the hot spot is prevented and various effects are obtained, including improvement of the selectivity.

If a five-valent antimony-containing compound is used as a source of antimony which is an ingredient of the catalytic active substance, the most suitable reaction temperature of the catalyst at a final stage becomes higher than a case where a three-valent antimony-containing compound is used.

Such effects are particularly notable under high load reaction conditions such as high gas concentration of o-xylene and/or naphthalene so that productivity can be very enhanced.

By using the catalyst of this invention, phthalic anhydride can be manufactured at high selectivity from o-xylene and/or naphthalene. The operations of heat treatment and distillation to obtain phthalic anhydride product are facilitated, and products of higher quality may be obtained at lower cost as compared with conventional methods.

The catalyst of this invention is durable, and accordingly long-term stable operation is possible industrially. Even under high load reaction conditions such as high concentration of material gas flow and even under high temperature conditions such as 380 °C or more, phthalic anhydride is produced with high selectivity, and even if the catalyst is used for a long period of time, it is durable and the productivity of phthalic anhydride is very much enhanced. Accordingly, the catalyst of the invention is extremely useful for producing phthalic anhydride.

BRIEF DESCRIPTION OF THE DRAWINGS

Fig. 1 is a chart showing the result from X-ray diffraction analysis of the catalyst E obtained from the example 2 in the region of a 10 to 90° diffraction angle.

Fig. 2 is a chart showing the result from X-ray diffraction analysis of the catalyst G obtained from the comparative example 2 in the region of a 10 to 90° diffraction angle.

Fig. 3 is a chart showing the result from X-ray diffraction analysis of a catalyst composed of only vanadium and titanium in the region of a 26 to 36° diffraction angle.

Fig. 4 is a chart showing the result from X-ray diffraction analysis of the catalyst G obtained from the comparative example 2 in the region of a 26 to 36° diffraction angle.

Fig. 5 is a chart showing the result from X-ray diffraction analysis of the catalyst E obtained from the example 2 in the region of a 26 to 36° diffraction angle.

DESCRIPTION OF THE PREFERRED EMBODIMENTS

Hereinafter, the present invention is illustrated by the following Examples of some preferred embodiments in comparison with Comparative examples.

Example 1

Preparation of catalyst

After mixing 80 % concentrated sulfuric acid with ilmenite and carrying out sufficient reaction, an aqueous solution of titanium sulfate was obtained by dilution with water. Iron pieces as reducing agent were added to this, and the iron content from the ilmenite was reduced to ferrous ions; after cooling, ferrous sulfate was precipitated and separated. Into the obtained aqueous solution of titanium sulfate, steam heated to 150 °C was blown, and hydrous titanium oxide was settled. It was washed with water, pickled and washed again with water, and was calcined at 800 °C for 4 hours in a passing air flow. It was crushed by jet air stream to obtain anatase type titanium dioxide (hereinafter, sometimes called simply titanium oxide) with an average particle size of about 0.5 μm and specific surface area of 22 m²/g.

In 6, 400 cm³ of deionized water, 200 g of oxalic acid was dissolved, and 47.24 g of ammonium metavanadate, 5.95 g of ammonium dihydrogen phosphate, 18.67 g of niobium chloride, 8.25 g of cesium sulfate, and 45.91 g of antimony pentoxide (average particle size: 20 μ m) were added and stirred. To the obtained solution, 1,800 g of titanium oxide was added, and was stirred by emulsifying machine to prepare

a catalyst slurry.

In a stainless steel rotary furnace of 35 cm diameter and 80 cm length which can be heated from outside, 2,000 cm³ of SiC self-sintered carrier of spherical form with diameter of 6 mm and apparent porosity of 35 % was charged, and while rotating the furnace preheated to 200 to 250 °C, the slurry was sprayed on to the carrier the catalytic active substance was thus supported at a rate of 8 g per 100 cc carrier. Afterwards, in passing air, it was calcined in an electric oven for 6 hours at 580 °C, to prepare catalyst A.

Table 1 shows the composition of catalyst A, the ratio in the catalytic active substance layer (% by volume) of the pore volume occupied by pores of 0. 15 to 0. 45 μ m diameter to the total fine pore volume occupied by pores of 10 μ m or less diameter, and the average particle size and specific surface area of the titanium oxide used in preparation of the catalyst (these are collectively called as catalyst characteristics, hereinafter). The ratio of the pore volume occupied by pores of 0. 15 to 0.45 μ m diameter to the total fine pore volume is determined from the pore distribution measured by a mercury injection porosimeter.

Catalyst B was prepared as for catalyst A, except that the content of ammonium dihydrogen phosphate was 23.82 g. The catalyst characteristics of catalyst B are shown in Table 1. The phosphorus content in catalyst B was higher than that in catalyst A, and the activity of catalyst B was higher than that of catalyst A.

Oxidation Reaction

Into an iron reaction tube of 25 mm inside diameter and 3 m length immersed in a molten salt bath kept at 390 °C catalyst B was charged as second stage catalyst to a height of 1 m at the material gas outlet end, then catalyst A as first stage catalyst was charged to a height of 1.5 m at the inlet.

o-Xylene was mixed at a ratio of 85 g/Nm³ (synthetic gas) with synthetic gas comprising 10 % by volume of oxygen, 10 % by volume of steam and 80 % by volume of nitrogen, and this mixture was led into the upper inlet of the reaction tube at a space velocity (SV) of 2,500 hr⁻¹ (STP) to oxidize the o-xylene.

At the beginning of reaction and 3 months after start of reaction, the yield of phthalic anhydride was measured, and the results are shown in Table 2. The conversion rate of o-xylene is nearly 100 %, and this yield can be regarded as the selectivity to phthalic anhydride.

Comparative example 1

Catalyst C and catalyst D were prepared as in Example 1 (preparation of catalyst) except that 36.73 g of antimony trioxide was used instead of 45.91 g of antimony pentoxide and the addition amount of cesium sulfate was 10.61 g; the oxidation reaction was conducted as in Example 1 (oxidation reaction). The catalyst characteristics of catalysts C and D are shown in Table 1 and results from oxidation reaction in Table 2.

Example 2

Catalyst E and catalyst F were prepared as in Example 1 (preparation of catalyst) except that 5.38 g of silver nitrate was also added and the addition amount of cesium sulfate was 5.90 g; the oxidation reaction was conducted as in Example 1 (oxidation reaction). The catalyst characteristics of catalysts E and F are shown in Table 1 and results from oxidation reaction in Table 2.

Comparative example 2

Catalyst G and catalyst H were prepared as in Example 1 (preparation of catalyst) except that 5.38 g of silver nitrate was also added and 36.73 g of antimony trioxide was used instead of 45.91 g of antimony pentoxide; the oxidation reaction was conducted as in Example 1 (oxidation reaction). The catalyst characteristics of catalysts G and H are shown in Table 1 and results from oxidation reaction in Table 2.

With respect to the catalysts E and G which were, respectively, obtained from the example 2 and comparative example 2, difference between the crystal structures of antimony in the catalysts was examined by X-ray diffraction analysis (XRD) using Cu-K α .

A main component in both catalysts E and G is anatase type TiO_2 and, as seen in both Figs. 1 and 2, large peaks due to the anatase type TiO_2 were detected in X-ray diffraction analyses of the catalysts E and G.

Therefore, in order to investigate the difference between five-valent antimony and three-valent antimony, the measurement was carried out with a raised detection sensitivity in a region where a peak due to the anatase type TiO_2 is absent (the diffraction angle 2θ is in a range of from 26° to 36°). In Table 3, are shown the peak positions (diffraction angle 2θ) of X-ray diffraction analysed in this region due to the antimony compounds having the five-valent and three-valent as well as due to V_2O_5 and Ag_2O . Meanwhile, the numeral values in parentheses in Table 3 represents relative intensities of the peaks.

For comparison, a catalyst composed of only vanadium and titanium was prepared and, when measurement was carried out in the region where the diffraction angle 2θ is in a range of from 26° to 36° , only a peak due to vanadium pentoxide (V_2O_5) was observed as seen in Fig. 3.

As seen in Fig. 4, in the catalyst G in which antimony trioxide (Sb_2O_3) was used, a large peak appeared at $2\theta = 27.1^\circ$ and another peak appeared at $2\theta = 35.4^\circ$. From these facts and the data in Table 3, antimony is thought to exist in a state near the form of Sb_2O_4 .

As seen in Fig. 5, in the catalyst E in which antimony pentoxide (Sb_2O_5) was used, a large peak appeared at $2\theta = 29.9^\circ$ and other peaks appeared at $2\theta = 28.6^\circ$ and 34.7° . From these facts and the data in Table 3, antimony is thought to exist in a state near the form of Sb_6O_{13} . However, there remain the peaks due to Sb_2O_5 at $2\theta = 27.1^\circ$, 28.9° and 34.3° .

From the forementioned, the effect of using a five-valent antimony-containing compound as a antimony source may be thought to be due to Sb_6O_{13} , but if there is used Sb_6O_{13} which was led from Sb_2O_5 by calcining it beforehand at a temperature of 700°C (no change in the surface area), the effect of present invention is not attained and a catalyst of high activity for a low temperature reaction is only obtained.

Example 3

Ilmenite and 80 % concentrated sulfuric acid were mixed and allowed to react sufficiently, then the product was diluted with water to obtain an aqueous solution of titanium sulfate. Iron pieces were added as reducing agent, and the iron content from the ilmenite was reduced to ferrous ions; after cooling, ferrous sulfate was precipitated and separated. Into the obtained aqueous solution of titanium sulfate, steam heated to 150°C was blown, and hydrous titanium oxide was settled. It was washed with water, pickled, and washed again with water, and was calcined at 700°C for 4 hours in a passing air flow. It was crushed by jet air stream, and anatase type titanium dioxide with specific surface area of $33\text{ m}^2/\text{g}$ measured by the BET method and average particle size of about $0.45\text{ }\mu\text{m}$ was obtained.

In 6,400 cc of deionized water, 900 g of oxalic acid was dissolved, and to this aqueous solution, 408.50 g of ammonium metavanadate, 10.30 g of ammonium dihydrogen phosphate, 17.22 g of niobium chloride, 4.08 g of cesium sulfate, 3.92 g of potassium sulfate, and 52.93 g of antimony pentoxide (average particle size: $20\text{ }\mu\text{m}$) were added and sufficiently stirred. To the obtained solution, 1,800 g of titanium oxide (which was the above-obtained anatase type titanium dioxide) was added, and the mixture was stirred by emulsifying machine to prepare a catalyst slurry.

Using this slurry, the catalytic active substance was supported as in Example 1 at a supporting rate of 8.0 g per 100 cc of carrier, followed by calcining in passing air in an electric oven at 560°C for 6 hours to prepare catalyst I.

Catalyst J was prepared as for catalyst I, except that the amount for use of ammonium dihydrogen phosphate was 30.89 g.

Oxidation reaction

Into an iron reaction tube of 25 mm inside diameter and 3 m length immersed in a molten salt bath kept at 395°C , catalyst J was charged as second stage catalyst to a height of 1 m, then catalyst I as first stage catalyst to a height of 1.5 m; naphthalene which was mixed at a ratio of 85 g/ Nm^3 (synthetic gas) with synthetic gas comprising 10 % by volume of oxygen 10 % by volume of steam and 80 % by volume of nitrogen was introduced into the upper part of the reaction tube at a space velocity of $2,500\text{ hr}^{-1}$ (STP) to perform the oxidation. Results are shown in Table 2.

Comparative example 3

Catalyst K and catalyst L were prepared as for catalysts I and J in Example 3 (preparation of catalyst), except that 42.34 g of antimony trioxide was used instead of 52.93 g of antimony pentoxide and the addition amount of cesium sulfate was 5.44 g; the oxidation reaction was performed as in Example 3 (oxidation reaction). The catalyst characteristics of catalysts K and L are shown in Table 1 and results from oxidation reaction in Table 2.

Example 4

Catalyst M and catalyst N were prepared as in Example 3 (preparation of catalyst), except that 31.04 g of silver nitrate was also added and the addition amount of cesium sulfate was 2.72 g; the oxidation reaction was performed as in Example 1 (oxidation reaction). The catalyst characteristics of catalysts M and N are shown in Table 1 and results from oxidation reaction in Table 2.

Comparative example 4

Catalyst O and catalyst P were prepared as in Example 3 (preparation of catalyst), except that 31.04 g of silver nitrate was also added and 42.34 g of antimony trioxide was used instead of 52.93 g of antimony pentoxide; the oxidation reaction was performed as in Example 1 (oxidation reaction). The catalyst characteristics of catalysts O and P are shown in Table 1 and results from oxidation reaction in Table 2.

Table I

Catalyst	Composition of catalyst (ratio by weight)				Titanium oxide		Pore volume ratio
	V ₂ O ₅ : TiO ₂ : Nb ₂ O ₅ : P ₂ O ₅ : Cs ₂ O : Ag ₂ O : Sb ₂ O ₅ : Sb ₂ O ₃ : K ₂ O				Average particle size	Specific surface area	
Example 1	A	2 : 98	0.5 : 0.2 : 0.35	— : 2.5 : —	0.5	22	86
	B	2 : 98	0.5 : 0.8 : 0.35	— : 2.5 : —	ditto	ditto	87
Comparative example 1	C	2 : 98	0.5 : 0.2 : 0.45	— : — : —	ditto	ditto	86
	D	2 : 98	0.5 : 0.8 : 0.45	— : — : 2.0	ditto	ditto	87
Example 2	E	2 : 98	0.5 : 0.2 : 0.25	0.2 : 2.5 : —	ditto	ditto	86
	F	2 : 98	0.5 : 0.8 : 0.25	0.2 : 2.5 : —	ditto	ditto	87
Comparative example 2	G	2 : 98	0.5 : 0.2 : 0.35	0.2 : — : —	ditto	ditto	86
	H	2 : 98	0.5 : 0.8 : 0.35	0.2 : — : 2.0	ditto	ditto	87
Example 3	I	15 : 85	0.4 : 0.3 : 0.15	— : 2.5 : —	0.45	33	80
	J	15 : 85	0.4 : 0.9 : 0.15	— : 2.5 : —	ditto	ditto	81
Comparative example 3	K	15 : 85	0.4 : 0.3 : 0.20	— : — : —	ditto	ditto	80
	L	15 : 85	0.4 : 0.9 : 0.20	— : — : 2.0	ditto	ditto	81
Example 4	M	15 : 85	0.4 : 0.3 : 0.10	1.0 : 2.5 : —	ditto	ditto	80
	N	15 : 85	0.4 : 0.9 : 0.10	1.0 : 2.5 : —	ditto	ditto	81
Comparative example 4	O	15 : 85	0.4 : 0.3 : 0.15	1.0 : — : —	ditto	ditto	80
	P	15 : 85	0.4 : 0.9 : 0.15	1.0 : — : 2.0	ditto	ditto	81

Average particle size: μm Specific surface area: m^2/g Pore volume ratio (Ratio of pore volume occupied by pores of 0.15 to 0.45 μm diameter to the total fine pore volume occupied by pores of 10 μm or less diameter): % by volume

Table 2

	Catalyst		Yield of phthalic anhydride (% by weight)	
	First stage	Second stage	Initial (°)	After 3 months (°)
Example 1	A	B	112.5 (392)	112.7 (390)
Comparative example 1	C	D	109.8 (392)	110.1 (389)
Example 2	E	F	113.8 (392)	114.0 (391)
Comparative example 2	G	H	111.7 (390)	112.0 (387)
Example 3	I	J	102.0 (394)	102.2 (388)
Comparative example 3	K	L	99.8 (392)	100.0 (387)
Example 4	M	N	103.9 (394)	104.2 (388)
Comparative example 4	O	P	102.0 (392)	102.3 (387)

(°) Molten salt temperature

Examples 1 and 2 and Comparative examples 1 and 2: o-xylene → phthalic anhydride

Examples 3 and 4 and Comparative examples 3 and 4: naphthalene → phthalic anhydride

Table 3

V ₂ O ₅	Sb ₂ O ₃	Sb ₂ O ₄
26.2° (90)	27.7° (100)	27.4° (100)
31.0° (65)	32.1° (40)	35.0° (70)
32.4° (35)	35.0° (11)	
33.3° (16)		
34.3° (40)		
36.0° (8)		
Sb ₂ O ₅	Sb ₅ O ₁₃	Ag ₂ O
27.2° (90)	28.6° (20)	32.7° (100)
29.0° (80)	29.9° (100)	
30.5° (80)	34.7° (30)	
33.6° (40)		
34.0° (80)		

Claims

1. A catalyst for producing phthalic anhydride by vapor phase catalytic oxidation of o-xylene and/or naphthalene with molecular oxygen or gas containing molecular oxygen, having supported on a heat-resistant inorganic carrier a catalytic active composition comprising [A] 1 to 20 parts by weight of vanadium oxide as V₂O₅ and 99 to 80 parts by weight of anatase type titanium dioxide with specific surface area of 10 to 60 m²/g as TiO₂ and [B], per 100 parts by total weight of [A], 0.01 to 1 part by weight of niobium as Nb₂O₅, 0.05 to 2 parts by weight of at least one element selected from potassium, cesium, rubidium and thallium as oxide, 0.2 to 1.2 parts by weight of phosphorus as P₂O₅, and 0.55 to 5.5 parts by weight as Sb₂O₅ of antimony obtained by using a five-valent antimony compound as an antimony source.
2. A catalyst according to claim 1 wherein [B] also includes 0.05 to 2 parts by weight of silver as Ag₂O per 100 parts by weight of [A].

3. A catalyst according to claim 1 or 2 wherein, in the catalytic active composition supported on the heat-resistant inorganic carrier, the pore volume occupied by pores of 0.15 to 0.45 μm diameter is 50% or more of the total fine pore volume occupied by pores of 10 μm or less diameter.
- 5 4. A process for producing phthalic anhydride by passing o-xylene and/or naphthalene together with molecular oxygen or gas containing molecular oxygen over catalyst having supported on a heat-resistant inorganic carrier a catalytic active composition comprising [A] 1 to 20 parts by weight of vanadium oxide as V_2O_5 and 99 to 80 parts by weight of anatase type titanium dioxide with specific surface area of 10 to 60 m^2/g as TiO_2 and [B], per 100 parts by total weight of [A], 0.01 to 1 part by weight of niobium as Nb_2O_5 , 0.05 to 2 parts by weight of at least one element selected from potassium, cesium, rubidium and thallium as oxide, 0.2 to 1.2 parts by weight of phosphorus as P_2O_5 , and 0.55 to 5.5 parts by weight as Sb_2O_5 of antimony obtained by using a five-valent antimony compound as an antimony source.
- 10 5. A process according to claim 4 wherein [B] also includes 0.05 to 2 parts by weight of silver as Ag_2O per 100 parts by weight of [A].
6. A process according to claim 4 or 5 wherein, in the catalytic active composition supported on the heat-resistant inorganic carrier, the pore volume occupied by pores of 0.15 to 0.45 μm diameter is 50% or more of the total fine pore volume occupied by pores of 10 μm or less diameter.
- 20 7. A process according to claim 4 or 5 or 6 conducted in a reactor divided into two or more sections to make a plurality of reaction zones, different catalysts of controlled activity and according to any of claims 4 to 6 being disposed in the zones so that the catalytic activity increases from the raw material gas inlet of the reactor towards the outlet.
- 25 8. A method of making vanadium-titanium-based catalyst for vapour phase catalytic oxidation of o-xylene and/or naphthalene to phthalic anhydride, said catalyst having supported on a heat-resistant inorganic carrier a catalytic active composition comprising [A] 1 to 20 parts by weight of vanadium oxide as V_2O_5 and 99 to 80 parts by weight of anatase type titanium dioxide with specific surface area of 10 to 60 m^2/g as TiO_2 and [B], per 100 parts by total weight of [A], 0.01 to 1 part by weight of niobium as Nb_2O_5 , 0.05 to 2 parts by weight of at least one element selected from potassium, cesium, rubidium and thallium as oxide, 0.2 to 1.2 parts by weight of phosphorus as P_2O_5 , and 0.55 to 5.5 parts by weight as Sb_2O_5 of antimony characterized in that the method includes incorporating antimony into the catalytically active composition using a five-valent antimony compound as starting material.
- 30 9. A method according to claim 8 wherein [B] also includes 0.05 to 2 parts by weight of silver as Ag_2O per 100 parts by weight of [A].
- 35 10. A method according to claim 8 or 9 wherein, in the catalytic active composition supported on the heat-resistant inorganic carrier, the pore volume occupied by pores of 0.15 to 0.45 μm diameter is 50% or more of the total fine pore volume occupied by pores of 10 μm or less diameter.
- 40

Patentansprüche

- 45 1. Katalysator zur Herstellung von Phthalsäureanhydrid durch katalytische Dampfphasen-Oxidation von o-Xylol und/oder Naphthalin mit molekularem Sauerstoff oder einem molekularen Sauerstoff enthaltenden Gas, der auf einem hitzebeständigen anorganischen Träger eine katalytisch aktive Substanz aufweist, enthaltend
 - 50 (A) 1 bis 20 Gew.-Teile Vanadiumoxid als V_2O_5 und 99 bis 80 Gew.-Teile Titandioxid vom Anatase-Typ mit einem spezifischen Oberflächenbereich von 10 bis 60 m^2/g als TiO_2 und
 - (B) je 100 Teile des Gesamtgewichtes von (A), 0,01 bis 1 Gew.-Teil Niob als Nb_2O_5 , 0,05 bis 2 Gew.-Teile mindestens eines Elements ausgewählt aus Kalium, Caesium, Rubidium und Thallium als Oxide, 0,2 bis 1,2 Gew.-Teile Phosphor als P_2O_5 und 0,55 bis 5,5 Gew.-Teile Antimon als Sb_2O_5 , erhalten unter Verwendung einer 5-wertigen Antimonverbindung als Antimonquelle.
 - 55
2. Katalysator nach Anspruch 1, dadurch gekennzeichnet, daß (B) zusätzlich 0,05 bis 2 Gew.-Teile Silber als Ag_2O je 100 Gew.-teile von (A) enthält.

3. Katalysator nach Anspruch 1 oder 2, dadurch gekennzeichnet, daß in der katalytisch aktiven Substanz, die sich auf dem hitzebeständigen anorganischen Träger befindet, das Porenvolumen, das aus Poren mit einem Durchmesser von 0,15 bis 0,45 μm besteht, 50% oder mehr ausmacht als das gesamte feine Porenvolumen, das aus feinen Poren mit einem Durchmesser von 10 μm oder weniger besteht.

4. Verfahren zur Herstellung von Phthalsäureanhydrid, bei dem man o-Xylol und/oder Naphthalin zusammen mit molekularem Sauerstoff oder einem molekularen Sauerstoff enthaltenden Gas über einen Katalysator leitet, der auf einem hitzebeständigen anorganischen Träger eine katalytisch aktive Substanz aufweist, enthaltend

(A) 1 bis 20 Gew.-Teile Vanadiumoxid als V_2O_5 und 99 bis 80 Gew.-Teile Titandioxid vom Anatas-Typ mit einem spezifischen Oberflächenbereich von 10 bis 60 m^2/g als TiO_2 und

(B) je 100 Teile des Gesamtgewichtes von (A), 0,01 bis 1 Gew.-Teil Niob als Nb_2O_5 , 0,05 bis 2 Gew.-Teile mindestens eines Elements ausgewählt aus Kalium, Caesium, Rubidium und Thallium als Oxide, 0,2 bis 1,2 Gew.-Teile Phosphor als P_2O_5 und 0,55 bis 5,5 Gew.-Teile Antimon als Sb_2O_3 , erhalten unter Verwendung einer 5-wertigen Antimonverbindung als Antimonquelle.

5. Verfahren nach Anspruch 4, dadurch gekennzeichnet, daß (B) zusätzlich 0,05 bis 2 Gew.-Teile Silber als Ag_2O je 100 Gew.-Teile von (A) enthält.

6. Verfahren nach Anspruch 4 oder 5, dadurch gekennzeichnet, daß in der katalytisch aktiven Substanz, die sich auf dem hitzebeständigen anorganischen Träger befindet, das Porenvolumen, das aus Poren mit einem Durchmesser von 0,15 bis 0,45 μm besteht, 50% oder mehr ausmacht als das gesamte feine Porenvolumen, das aus feinen Poren mit einem Durchmesser von 10 μm oder weniger besteht.

7. Verfahren nach Anspruch 4 oder 5 oder 6, dadurch gekennzeichnet, daß man das Verfahren in einem Reaktor durchführt, der in zwei oder mehrere Sektionen unter Bildung einer Vielzahl von Reaktionszonen aufgeteilt ist, wobei in den Zonen unterschiedliche Katalysatoren von gesteuerter Aktivität und gemäß irgendeinem der Ansprüche 4 bis 6 angeordnet sind, so daß die katalytische Aktivität von dem Rohmaterialgas-Einlaß des Reaktors zum Auslaß ansteigt.

8. Verfahren zur Herstellung eines auf Vanadium-Titan basierenden Katalysators zur katalytischen Dampfphasen-Oxidation von o-Xylol und/oder Naphthalin zu Phthalsäureanhydrid, wobei der Katalysator auf einem hitzebeständigen anorganischen Träger eine katalytisch aktive Substanz aufweist, enthaltend

(A) 1 bis 20 Gew.-Teile Vanadiumoxid als V_2O_5 und 99 bis 80 Gew.-Teile Titandioxid vom Anatas-Typ mit einem spezifischen Oberflächenbereich von 10 bis 60 m^2/g als TiO_2 und

(B) je 100 Teile des Gesamtgewichtes von (A), 0,01 bis 1 Gew.-Teil Niob als Nb_2O_5 , 0,05 bis 2 Gew.-Teile mindestens eines Elements ausgewählt aus Kalium, Caesium, Rubidium und Thallium als Oxide, 0,2 bis 1,2 Gew.-Teile Phosphor als P_2O_5 und 0,55 bis 5,5 Gew.-Teile Antimon als Sb_2O_3 , dadurch gekennzeichnet, daß man das Antimon in die katalytisch aktive Substanz einbringt, indem man eine 5-wertige Antimonverbindung als Ausgangsmaterial einsetzt.

9. Verfahren nach Anspruch 8, dadurch gekennzeichnet, daß (B) zusätzlich 0,05 bis 2 Gew.-Teile Silber als Ag_2O je 100 Gew.-teile von (A) enthält.

10. Verfahren nach Anspruch 8 oder 9, dadurch gekennzeichnet, daß in der katalytisch aktiven Substanz, die sich auf dem hitzebeständigen anorganischen Träger befindet, das Porenvolumen, das aus Poren mit einem Durchmesser von 0,15 bis 0,45 μm besteht, 50% oder mehr ausmacht als das gesamte feine Porenvolumen, das aus feinen Poren mit einem Durchmesser von 10 μm oder weniger besteht.

Revendications

1. Un catalyseur pour la production d'anhydride phtalique par oxydation catalytique en phase vapeur du o-xylène et/ou du naphthalène avec l'oxygène moléculaire ou un gaz contenant de l'oxygène moléculaire, qui comporte, supportée par un support minéral réfractaire, une composition catalytique active comprenant [A] 1 à 20 parties en poids d'oxyde de vanadium sous forme de V_2O_5 et 99 à 80 parties en poids de bioxyde de titane du type anatase ayant une surface spécifique de 10 à 60 m^2/g sous forme de TiO_2 et [B], pour 100 parties du poids total de [A], 0,01 à 1 partie en poids de niobium sous forme de Nb_2O_5 , 0,05 à 2 parties en poids d'au moins un élément choisi parmi le potassium, le

césium, le rubidium et le thallium sous forme d'oxyde, 0,2 à 1,2 partie en poids de phosphore sous forme de P_2O_5 et 0,55 à 5,5 parties en poids d'antimoine, sous forme de Sb_2O_5 , obtenu en utilisant un composé d'antimoine pentavalent comme source d'antimoine.

- 5 2. Un catalyseur selon la revendication 1, dans lequel [B] contient également 0,05 à 2 parties en poids d'argent sous forme de Ag_2O pour 100 parties en poids de [A].
3. Un catalyseur selon la revendication 1 ou 2, dans lequel, dans la composition catalytique active supportée par le support minéral réfractaire, le volume poreux occupé par des pores de 0,15 à 0,45 μm de diamètre représente 50 % ou plus du volume poreux fin total occupé par les pores de 10 μm ou moins de diamètre.
- 10 4. Un procédé pour produire de l'anhydride phtalique en faisant passer du o-xylène et/ou du naphthalène avec de l'oxygène moléculaire ou un gaz contenant de l'oxygène moléculaire sur un catalyseur qui comporte, supportée par un support minéral réfractaire, une composition catalytique active comprenant [A] 1 à 20 parties en poids d'oxyde de vanadium sous forme de V_2O_5 et 99 à 80 parties en poids de bioxyde de titane du type anatase ayant une surface spécifique de 10 à 60 m^2/g sous forme de TiO_2 et [B], pour 100 parties du poids total de [A], 0,01 à 1 partie en poids de niobium sous forme de Nb_2O_5 , 0,05 à 2 parties en poids d'au moins un élément choisi parmi le potassium, le césium, le rubidium et le thallium sous forme d'oxyde, 0,2 à 1,2 partie en poids de phosphore sous forme de P_2O_5 et 0,55 à 5,5 parties en poids d'antimoine, sous forme de Sb_2O_5 , obtenu en utilisant un composé d'antimoine pentavalent comme source d'antimoine.
- 15 5. Un procédé selon la revendication 4, dans lequel [B] contient également 0,05 à 2 parties en poids d'argent sous forme de Ag_2O pour 100 parties en poids de [A].
- 25 6. Un procédé selon la revendication 4 ou 5, dans lequel, dans la composition catalytique active supportée par le support minéral réfractaire, le volume poreux occupé par des pores de 0,15 à 0,45 μm de diamètre représente 50 % ou plus du volume poreux fin total occupé par les pores de 10 μm ou moins de diamètre.
- 30 7. Un procédé selon la revendication 4, 5 ou 6, conduit dans un réacteur divisé en deux ou plusieurs sections pour constituer plusieurs zones réactionnelles, différents catalyseurs d'activité déterminée et selon l'une quelconque des revendications 4 à 6 étant disposés dans les zones de telle manière que l'activité catalytique augmente depuis l'entrée de matière première gazeuse du réacteur vers la sortie.
- 35 8. Un procédé de préparation d'un catalyseur à base de vanadium-titane pour l'oxydation catalytique en phase vapeur du o-xylène et/ou du naphthalène en anhydride phtalique, ledit catalyseur comportant, supportée par un support minéral réfractaire, une composition catalytique active comprenant [A] 1 à 20 parties en poids d'oxyde de vanadium sous forme de V_2O_5 et 99 à 80 parties en poids de bioxyde de titane du type anatase ayant une surface spécifique de 10 à 60 m^2/g sous forme de TiO_2 et [B], pour 100 parties du poids total de [A], 0,01 à 1 partie en poids de niobium sous forme de Nb_2O_5 , 0,05 à 2 parties en poids d'au moins un élément choisi parmi le potassium, le césium, le rubidium et le thallium sous forme d'oxyde, 0,2 à 1,2 partie en poids de phosphore sous forme de P_2O_5 et 0,55 à 5,5 parties en poids d'antimoine, sous forme de Sb_2O_5 , caractérisé en ce que le procédé comprend l'incorporation de l'antimoine dans la composition catalytiquement active en utilisant comme matière de départ un composé d'antimoine pentavalent.
- 40 9. Un procédé selon la revendication 8, dans lequel [B] contient également 0,05 à 2 parties en poids d'argent sous forme de Ag_2O pour 100 parties en poids de [A].
- 45 10. Un procédé selon la revendication 8 ou 9, dans lequel, dans la composition catalytique active supportée par le support minéral réfractaire, le volume poreux occupé par des pores de 0,15 à 0,45 μm de diamètre représente 50 % ou plus du volume poreux fin total occupé par les pores de 10 μm ou moins de diamètre.
- 55

Fig. 1

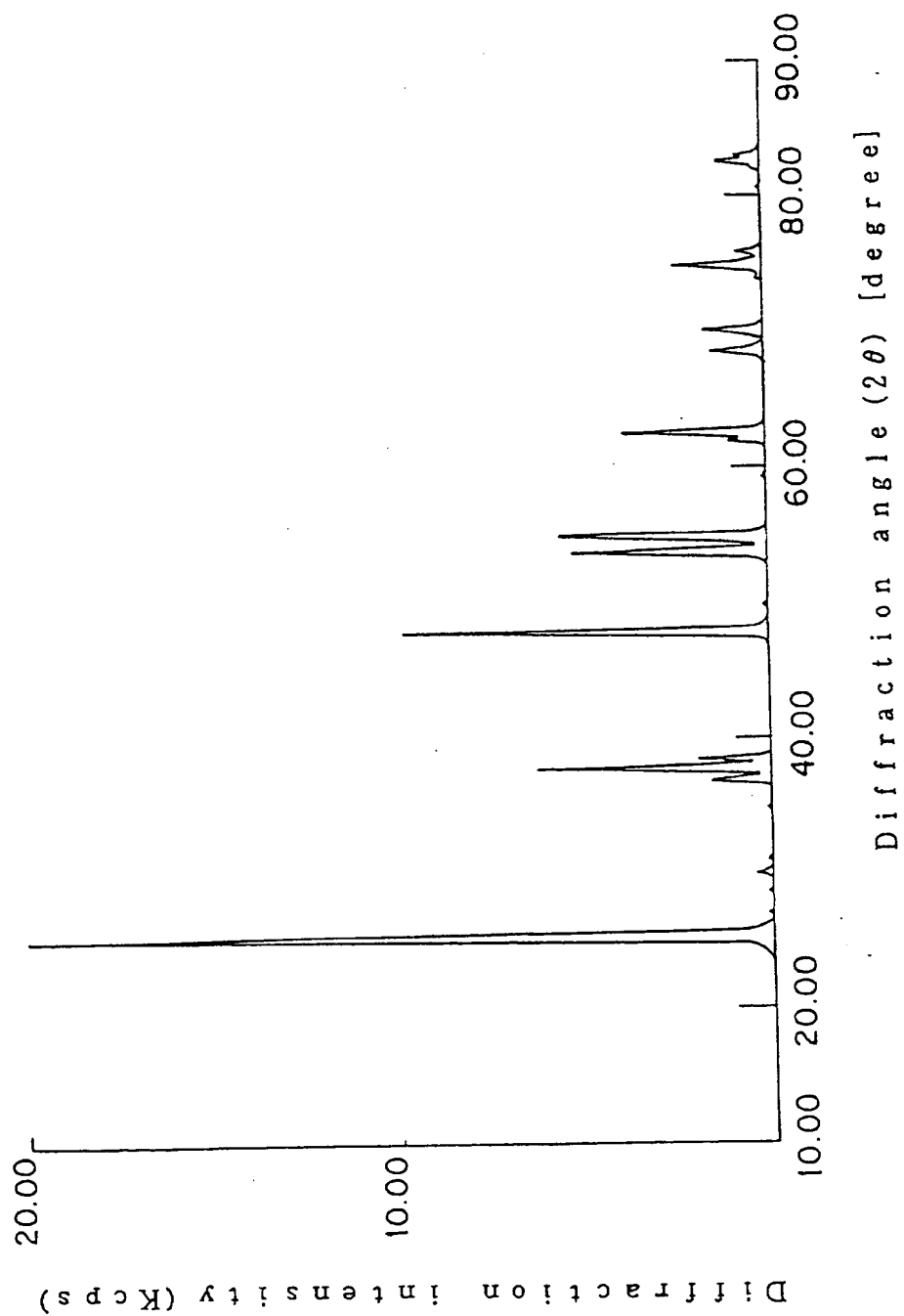


Fig. 2

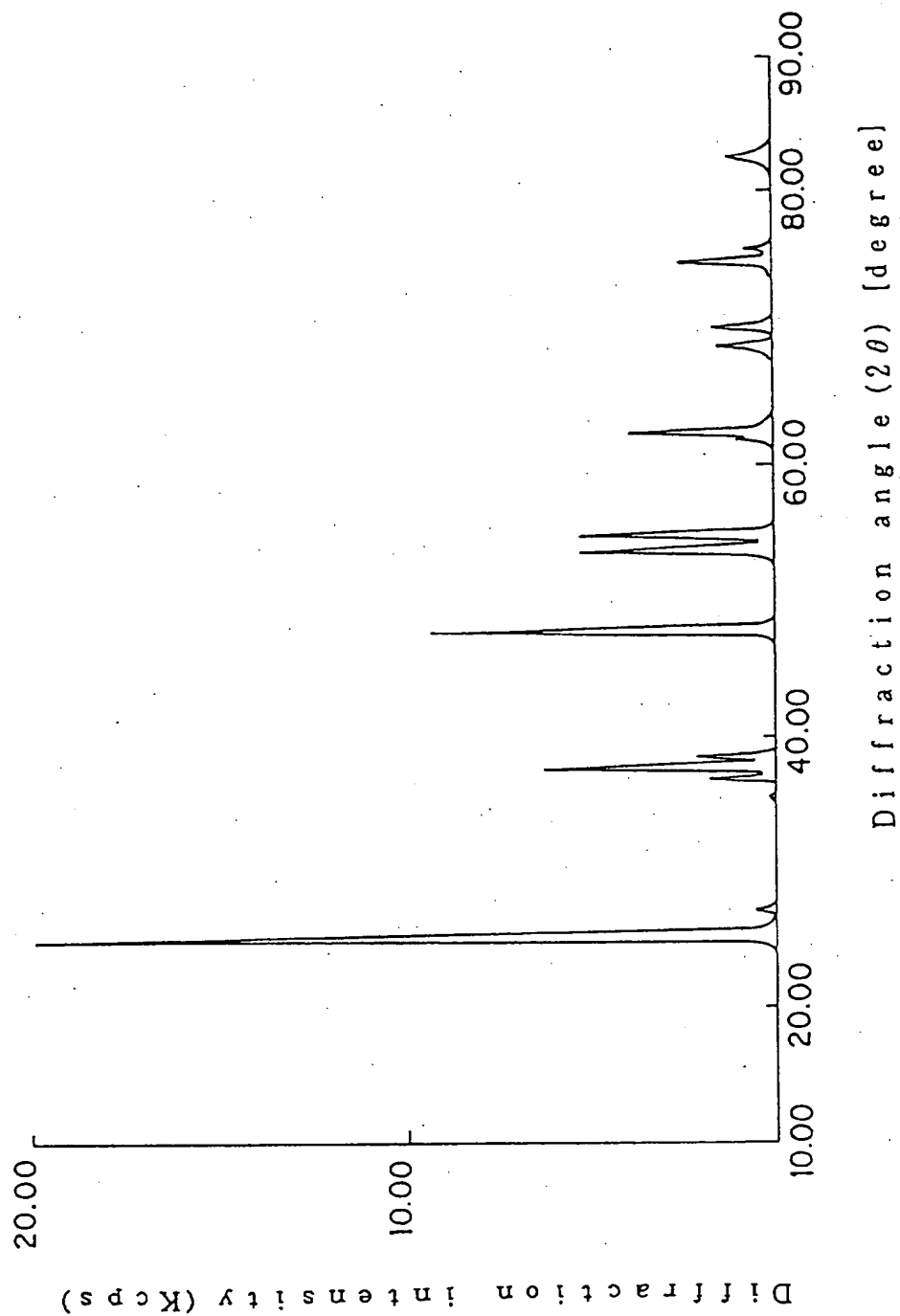


Fig. 3

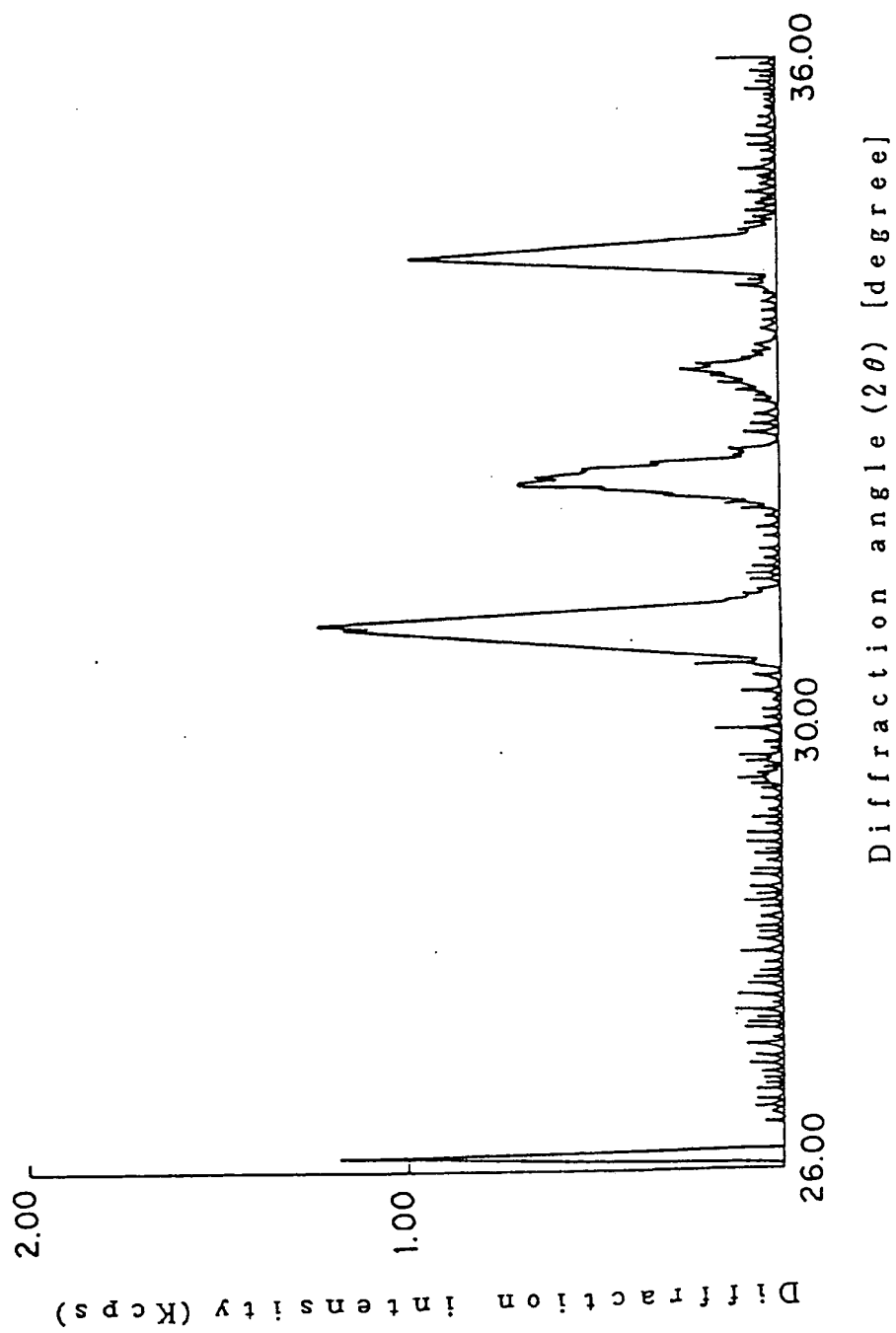


Fig. 4

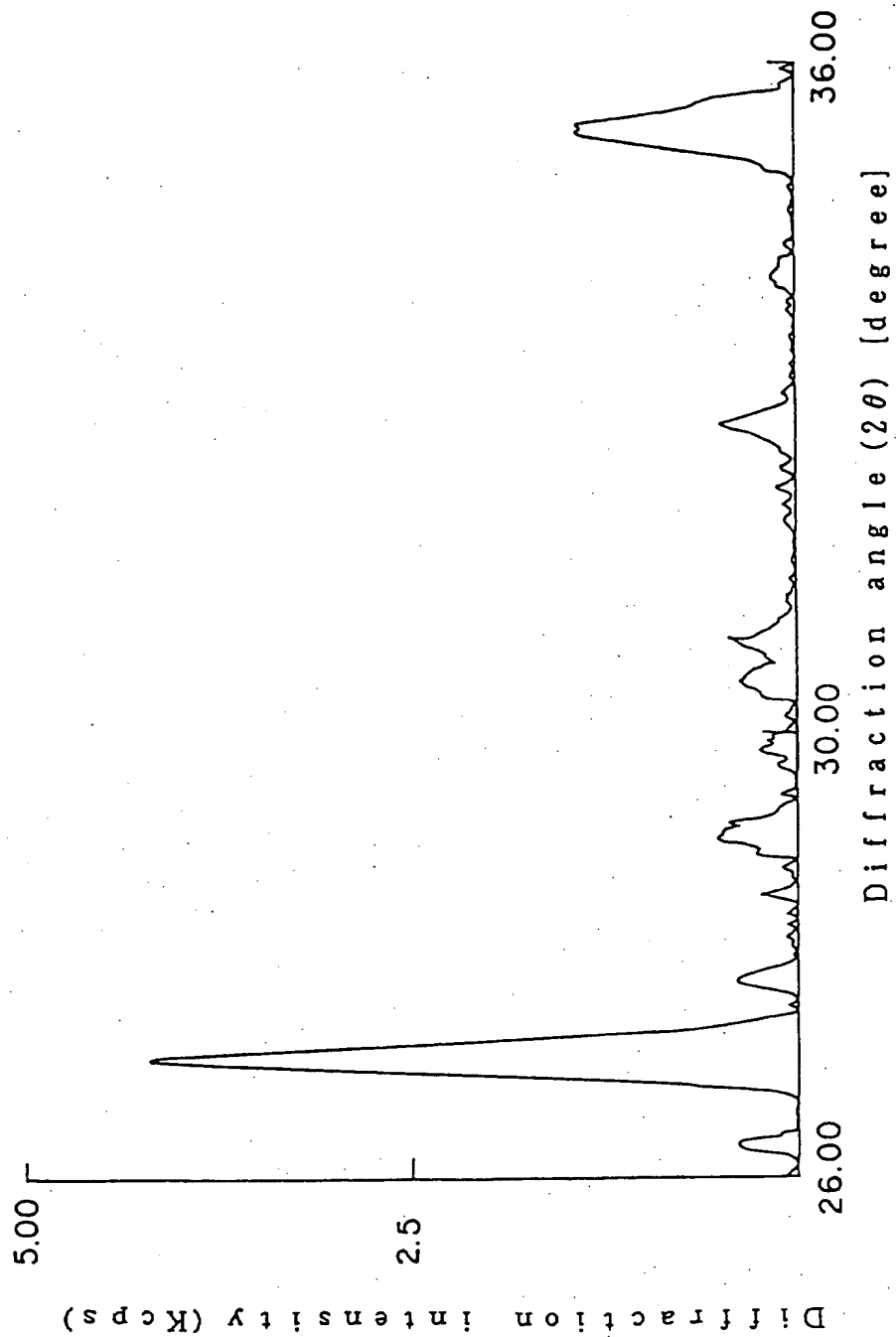


Fig. 5

